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on October 6, 2000

Lori J. Larson

Name and Reg. No. of Attorney

Signature

Date of Signature

EL398545056US

Docket No.: 00-625Anticipated Classification of
this application:

Class _____ Subclass _____

Prior Application:

Examiner: T. TranArt Unit: 1741

jc915 U.S. PTO

09/684173



10/06/00

THE COMMISSIONER OF PATENTS AND TRADEMARKS
Washington, D.C. 20231

SIR: This is a request for filing a () Continuation
(XX) Divisional application under 37 CFR 1.60, of pending prior
application Serial No. 09/324,574 filed on June 2, 1999 of
James R. Kittrell for TWO STAGE PROCESS AND APPARATUS FOR
PHOTOCATALYTIC AND CATALYTIC CONVERSION OF CONTAMINANTS.

1. (XX) Enclosed is a copy of the prior application, including
the oath or declaration as originally filed and an
affidavit or declaration verifying it as a true copy.
2. (XX) The filing fee is calculated below:

PRIOR TO CALCULATING THE FILING FEE DUE, SEE ITEM NO. 8

For	No. Filed	No. Extra	SMALL ENTITY		OTHER THAN A SMALL ENTITY	
			Rate	Fee	Rate	Fee
Basic Fee				\$ 355		\$ 710
Total Claims 2	-20 =	--	x 9	\$	x 18	\$ --
Indep Claims 1	- 3 =	--	x 40	\$	x 80	\$ --
Multiple Dependent Claim () Presented			+135	\$	+270	\$ --
			TOTAL	\$	TOTAL	\$ 710

3. () Please charge my Deposit Account No. 02-0184 in the
amount of \$ _____. A duplicate copy of this sheet
is enclosed.
4. (XX) A check in the amount of \$ 710.00 to cover the filing
fee is enclosed.
5. (XX) The Commissioner is hereby authorized to charge payment
of the following fees associated with this
communication or credit any overpayment to Deposit
Account No. 02-0184. A duplicate copy of this sheet is
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 - a. (XX) Any additional filing fees required under 37
CFR 1.16.
 - b. (XX) Any patent application processing fees under
37 CFR 1.17.
6. (XX) The Commissioner is hereby authorized to charge payment
of the following fees during the pendency of this
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Account No. 02-0184. A duplicate copy of this sheet is
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 - a. (XX) Any patent application processing fees under
37 CFR 1.17
 - b. (XX) Any filing fees under 37 CFR 1.16 for
presentation of extra claims.


005001-2640500

- 005007-2246560
7. () A verified statement to establish small entity status under 37 CFR 1.9 and 37 CFR 1.27.
8. (XX) Cancel in this application original Claims 1-24 of the prior application before calculating the filing fee.
9. () Amend the specification by inserting before the first line the sentence: --This is a () Continuation, () Division, of application Serial No. , filed .--.
10. () Transfer the drawings from the prior application to this application and abandon said prior application as of the filing date accorded this application. A duplicate copy of this sheet is enclosed for filing in the prior application file.
11. () New formal drawings are enclosed.
12. () Priority of application Serial No. , filed on in is claimed under 35 U.S.C. §119.
13. () The certified copy has been filed in prior application Serial No. , filed .
14. (XX) The prior application is assigned of record to KSE, Inc.
15. (XX) The power of attorney in the prior application is to Robert H. Bachman (19,374), Gregory P. LaPointe (28,395), Barry L. Kelmachter (29,999) and George A. Coury (34,309).
- (XX) a. The power appears in the original papers in the prior application.
- () b. Since the power does not appear in the original papers, a copy of the power in the prior application is enclosed.
- (XX) c. Address all future communications to Gregory P. LaPointe, Bachman & LaPointe, P.C. 900 Chapel Street, Suite 1201, New Haven, CT 06510-2802.
16. (XX) A Preliminary Amendment is enclosed.
17. (XX) I hereby verify that the attached papers are a true copy of prior application Serial No. 09/324,574 as originally filed on June 2, 1999.

The undersigned declares further that all statements made herein of his own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under section 1001 of Title 18 of the United States Code and that such willful false statement may jeopardize the validity of the application or any patent issuing thereon.

October 6, 2000

Address of signator:
Bachman & LaPointe, P.C.
900 Chapel Street, Suite 1201
New Haven, CT 06510-2802


Gregory P. LaPointe
Attorney of Record
Reg. No. 28,395

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Applicant : JAMES R. KITTRELL Docket No.: 00-625
Serial No.: Examiner :
Filed : Art Unit :
For : TWO STAGE PROCESS AND APPARATUS
FOR PHOTOCATALYTIC AND CATALYTIC
CONVERSION OF CONTAMINANTS

Suite 1201
900 Chapel Street
New Haven, CT 06510-2802

PRELIMINARY AMENDMENT

Hon. Commissioner of Patents & Trademarks
United States Patent & Trademark Office
Washington, D.C. 20231

Dear Sir:

In the above-identified application for United States patent,
please amend as follows.

IN THE SPECIFICATION

On Page 2, before the "BACKGROUND OF THE INVENTION" please insert
the following new paragraph:

--CROSS-REFERENCE TO RELATED APPLICATION

The instant application is a divisional of Application Serial No.
09/324,574 filed June 2, 1999.--

IN THE CLAIMS

Please cancel claims 25 and 26, the only claims pending in the
instant application, and add new claims 27-30 as follows.

--27. A catalyst for converting contaminants in a gas stream comprises from about 0.1 wt.% to about 70 wt.% silica, from about 30 wt.% to about 90 wt.% titania, and from about 10 wt.% to about 50 wt.% tungsten oxide.

28. A catalyst according to claim 27, wherein said tungsten oxide is present in an amount of between about 20 wt.% to about 30 wt.%.

29. A catalyst according to claim 27, wherein said catalyst further includes an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 wt.% to about 5.0 wt.%.

30. A catalyst according to claim 28, wherein said catalyst further includes an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 wt.% to about 5.0 wt.%.--

REMARKS

The instant application is a divisional of Application Serial No. 09/324,574 filed June 2, 1999. An early action on the merits is respectfully requested.

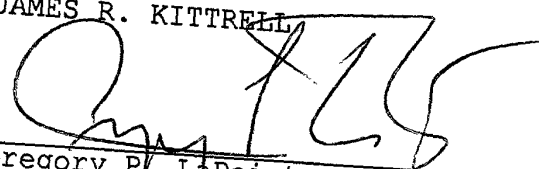
If any fees are required in connection with this case, it is respectfully requested that they be charged to Deposit Account

No. 02-0184.

Respectfully submitted,

JAMES R. KITTRELL

By


Gregory P. LaPointe
Attorney for Applicant
Reg. No. 28,395
Tel: (203) 777-6628
Fax: (203) 865-0297

Date: October 6, 2000

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on October 6, 2000

(Date of Deposit)

Lori J. Larson

Name and Reg. No. of Attorney



Signature

Oct 6 2000

Date of Signature

EL398545056US

APPLICATION FOR LETTERS PATENT

TO ALL WHOM IT MAY CONCERN:

BE IT KNOWN THAT James R. Kittrell, a citizen of the United States of America and resident of the State of Massachusetts, has invented certain new and useful improvements in TWO STAGE PROCESS AND APPARATUS FOR PHOTOCATALYTIC AND CATALYTIC CONVERSION OF CONTAMINANTS of which the following is a specification.

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on October 6, 2000
(Date of Deposit)
Lori J. Larson
Name and Reg. No. of Attorney
Lori J. Larson
Signature
Oct 6, 2000
Date of Signature

Express Mail No. EL398545056US

BACKGROUND OF THE INVENTION

The present invention is drawn to a process and catalyst for destruction of contaminants in a gaseous stream (preferably air) into less harmful products by irradiating the contaminated air with ultraviolet light in a first photocatalytic stage wherein the photocatalyst is irradiated with ultraviolet light while in contact with the contaminated air to convert at least a portion of the contaminants into carbon dioxide. The contaminated air then is passed into a second catalytic stage, wherein the contaminant is exposed to a catalyst without further heating of the contaminated air. Surprisingly, it is found that the pretreatment in the first photocatalytic stage increases overall process efficiency, by efficiently releasing heat utilized by the catalytic stage and by producing intermediate species which are efficiently converted in the second catalytic stage without forming harmful byproducts.

In spite of decades of effort, a significant need remains for an advanced technology to control stationary source emissions of volatile organic compounds (VOCs) as for example benzene, chlorinated volatile organic compounds (CVOCs) as for example trichloroethylene, and toxic air pollutants (TAPs) as for example acrylonitrile. A particular need exists for technology which controls emissions from industrial processes

and other applications where VOCs and TAPs are present in high flow rate air streams.

Pollution control in high flow rate air streams is becoming recognized as a major environmental control issue for the United States industrial community at large. For example, the control of emissions associated with solvent degreasing operations is necessary, including the emissions associated with exhaust ventilation fans. Also, air stripping of contaminated groundwater produces air emissions for which current technology provides no satisfactory solution. Catalytic combustors are available, but require processing tremendous volumes of air and result in uneconomic performance. Thermal incinerators require excessive supplemental fuel for dilute mixtures, and exhibit uncertain selectivity when CVOC's are involved. Gas membrane processes are only now emerging for gas separation, and are ill-suited for dilute mixtures. Pressure swing adsorption using zeolites or resins is not applicable to dilute mixtures, and rotating wheel adsorbers are uneconomic for such dilute concentrations of organics. Packed bed activated carbon adsorption is widely practiced, but creates a hazardous solid waste which is increasingly difficult to manage. Carbon regeneration by steam is costly, and is generally economic only for very large scale operations. Landfill options for spent carbon will

become more limited, as it involves transportation and disposal of hazardous wastes, particularly for CVOC applications.

Control of indoor air pollution is also of growing importance, with the objective of enhancing workplace environmental health and safety protection. The Occupational Safety and Health Administration (OSHA) is promulgating new regulations to reduce workplace exposure to indoor air contaminants such as CVOCs. Many CVOCs are particularly toxic. Certain CVOCs are suspected carcinogens, others are linked to possible birth defects, and still others are suspected active precursors in the destruction of the stratospheric ozone layer. Of the 189 targeted air toxics in the Clean Air Act Amendments of 1990, about one-third of the compounds are chlorinated.

In spite of considerable efforts of researchers in the field, most UV photocatalysts exhibit shortcomings in catalyst activity, selectivity, and deactivation which limit their commercial utility for air pollution control.

Researchers have studied titania photocatalysis, although not achieving the benefits of the present invention. Raupp has reported titania photocatalysts for the UV oxidation of organics in air (see Raupp, G.B., et al., "Destruction of Organics in Gaseous Streams Over UV-Excited Titania", 85th

Annual Meeting, Air & Waste Management Association, Kansas City, June 21-26, 1992). The activity of a titania photocatalyst rapidly declines with time-on-stream with trichloroethylene (TCE) in air (see Raupp, G.B., "Photocatalytic Oxidation for Point-of-Use VOC Abatement in the Microelectronics Fabrication Industry", Air & Waste Management Association, 87th Annual Meeting, Cincinnati, Ohio, June 19-24, 1995). Ollis describes photocatalytic reactors and reports that TCE photocatalysts in air can lead to 75 ppm(v) of phosgene in the reactor product in the photocatalytic oxidation of organics over a thin titania bed (see Ollis, D.F., in Photocatalytic Purification and Treatment of Water and Air, 481-494, Elsevier, NY, 1993; and Peral, J. and D.F. Ollis, "Heterogeneous Photocatalytic Oxidation of Gas-Phase Organics for Air Purification", J. Catalysis, 136, 554-564, 1992). Pichat has reported great difficulty oxidizing aromatics in the gas phase with a titania photocatalyst (see Pichat, P., in Photoelectrochemistry, Photocatalysis and Photoreactors, 425-455, Reidel Publishing, Boston, 1985). Researchers at Purdue have investigated gas phase photocatalysis of TCE using titania on a concentric reactor wall around a UV light source (see Wang, K. and B.J. Marinas, in Photocatalytic Purification and Treatment of Water and Air, 733-737, Elsevier, 1993). They employed residence

times of over 6 seconds, and found evidence of byproducts, suspected to be phosgene. Teichner reports that byproduct formation with titania photocatalysts is the rule, not the exception (see Teichner, S.J. and N. Formenti, in Photoelectrochemistry, Photocatalysis and Photoreactors, 457-489, Reidel Pub, Boston, 1985). Nutech Energy Systems has disclosed titania impregnated on a fiberglass mesh (see U.S. Patent 4,892,712 issued January 9, 1990; U.S. Patent 4,966,759 issued October 30, 1990; and U.S. Patent 5,032,241 issued July 16, 1991). A technical paper on the Nutech technology disclosed a gas phase residence time of 8.4 seconds and evidence of byproducts formation up to 34 seconds residence time (see Al-Ekabi, H., et al., in Photocatalytic Purification & Treatment of Water and Air, 719-725, Elsevier, NY, 1993). The University of Wisconsin investigators have used 100 second residence time for photocatalytic destruction of gas phase TCE using titania (see Yamazaki-Nishida, S., et al., "Gas Phase Photocatalytic Degradation on Titania Pellets of Volatile Chlorinated Organic Compounds from a Soil Vapor Extraction Well", J. Soil Contamination, Sept., 1994; Fu, X., W.A. Zeltner, and M.A. Anderson, "The Gas-Phase Photocatalytic Mineralization of Benzene on Porous Titania-Based Catalysts", Applied Catalysis B: Environmental, 6, 209-224, 1995; and U.S. Patent 5,035,078 issued July 30, 1991).

Titania has been used for decades in photocatalysis (see Formenti, M., et al., "Heterogeneous Photocatalysis for Oxidation of Paraffins", Chemical Technology 1, 680-686, 1971 and U.S. Patent 3,781,194 issued December 25, 1973). Due to the high absorption of UV light by titania, about 99% of the incident UV radiation is absorbed within the first 4.5 microns on titania (see Peral, J. and D.F. Ollis, "Heterogeneous Photocatalytic Oxidation of Gas-Phase Organics for Air Purification", J. Catalysis, 136, 554-564, 1992). Hence, the patent literature discloses methods to distribute the titania in thin layers in an attempt to overcome this deficiency. In 1973, Teichner disclosed a method of using titania supported on a matrix in a thin film reactor to oxidize hydrocarbons to aldehydes and ketones (see U.S. Patent 3,781,194 issued December 25, 1973). Titania has been deposited in thin layers on glass wool, on a ceramic membrane, and the wall of a reactor (see U.S. Patent 4,888,101 issued December 19, 1989; U.S. Patent 5,035,078 issued July 30, 1991; U.S. Patent 4,966,665 issued October 30, 1990). Raupp has disclosed titania for photocatalytic use when mixing two gas streams, and included thin bed catalytic reactors (see U.S. Patent 5,045,288 issued September 3, 1991).

The requirement of thin film reactors is a major deficiency, leading to greatly increased cost and complexity

in commercial reactor construction. For example, a commercial reactor may require 500 to 1000, or more, UV lamps. Methods to provide illumination of thin films of catalyst require a huge surface area for impingement of incident UV radiation. For example, one common method of deployment of catalyst in a thin film is to coat the interior of a reactor tube, which surrounds a UV lamp in the centerline of the tube. This method, then, requires that 500 to 1000, or more, individual reactor tubes be constructed and assembled, which is costly and cumbersome. In addition, the flow must be equally split and balanced among the 500 to 1000, or more, reactor tubes in parallel operation, which is difficult and costly to accomplish and maintain. Further, to prevent the gas from bypassing the catalyst by preferentially flowing between the UV tube and the thin catalyst layer, the gap between the UV lamp and the catalyst must be very small or a turbulent promoting flow disruption must be inserted between the UV lamp and the catalyst. These lead to a very high pressure drop for the gas flowing through the reactor. Particularly for the large flow rates of gas in commercial reactors, this leads to high pressure drop, requiring both expensive gas compressors and a cooling device to remove the heat of compression of the gas. For these reasons, little or no commercial practice of thin film titania photocatalysts has been accomplished.

U.S. Patent 4,966,665 discloses the use of titanium dioxide as a photocatalyst for destruction of chlorine-containing organic compounds in an oxygen-bearing vent gas. The method was used in a system wherein the titanium dioxide was supported on the wall of a reactor through which the vent gas is passed. This is an ineffective reactor design for large gas flows, requiring a very large number of small diameter parallel tubes among which the flow must be equally balanced. Further, the cost of such a reactor is very high compared to a single large diameter reactor. Still further, when a vent gas containing 30 ppm TCE was contacted with titanium dioxide for 26 seconds, 90% destruction of TCE was obtained. However, the analysis of the reactor products revealed the formation of byproducts such as 4 ppm phosgene and 1 ppm carbon tetrachloride which are more hazardous than TCE.

U.S. Patent 5,045,288 discloses a method of removing organic contaminants from a gaseous stream, wherein a mixing step is conducted, combining (a) a gaseous oxygen bearing stream and (b) a contaminated stream. This mixture is then passed over a photocatalyst exposed to UV radiation of wavelength not greater than 600 nm. The reaction conditions must be preselected to prevent formation of a liquid phase on the catalyst. Only when the reactor comprises a body portion

having a window for passing visible light, the photocatalyst may be selected from the group consisting of titanium dioxide, zirconium oxide, antimony oxide, zinc oxide, stannic oxide, cerium oxide, tungsten oxide, and ferric oxide. The invention is deficient in that it requires mixing two streams, requires avoiding liquid phases, and requires a visible light window, all of which are impractical in commercial systems. Further, the catalyst compositions are not effective.

U.S. Patent 4,888,101 discloses a system for photocatalysis wherein a semiconductor is entrapped in a fiber mesh. U.S. Patents 4,892,712 and 4,966,759 disclose a photocatalyst for detoxifying organic pollutants from a fluid, comprising a substrate in the form of a plurality of layers of a filamentous, fibrous, or stranded base material, and a photoreactive metal semiconductor material bonded to surfaces of said layers. The photoreactive material is selected from anatase, CdS, CdSe, ZnO₂, WO₃ and SnO₂. This disclosure is of limited value because the substrate leads to a high pressure drop under conditions providing intimate contacting of the fluid flowing through or by the substrate. Further, the base material is generally of low surface area, leading to poor overall reactor performance. Still further, the design also generally requires a sleeve of this material around each bulb, leading to a costly reactor design. Finally, the

photoreactive metal semiconductors are not of high photocatalytic activity. U.S. Patent 5,032,241 provides a similar system for killing microorganisms in a fluid.

U.S. Patent 4,780,287 discloses a method of decomposing volatile organic halogenated compounds by passing the gas through silica gel or quartz chips, and the bed is thereafter irradiated with UV light. Ozone or hydrogen peroxide are added to an aqueous phase. The system lost catalytic activity and required heating with nitrogen gas to restore the decomposing activity. Presumably, this loss of activity was due to the decomposition of the CVOC, rather than promoting its complete oxidation. U.S. Patent 4,941,957 discloses a method for decomposing CVOC's present in gases and aqueous solutions. The aqueous phase CVOC's are removed by volatilizing into a gaseous carrier. The gas was then passed through silica gel and simultaneously irradiated with UV light and/or exposing the bed to ozone. The system required a great excess of ozone, using 2% ozone to decompose TCE at air compositions of only 50 parts per billion (ppb) to 700 ppb, which is generally uneconomic.

Accordingly, it is a principle object of the present invention to provide a process for efficient destruction of contaminants in a gaseous stream such as air utilizing a two step process.

It is a further object of the present invention to provide a process as mentioned above which comprises a photocatalytic step followed by a catalytic step.

SUMMARY OF THE INVENTION

The foregoing objects are achieved by way of the present invention wherein a process comprises passing a contaminated gaseous stream through a photocatalytic stage and, thereafter, through a catalytic stage.

In accordance with the present invention the process for purifying a contaminated gas stream by conversion of the contaminants into less harmful products, comprises the steps of providing a photocatalytic stage having a photocatalyst and a source of UV radiation, providing a catalytic stage downstream of the photocatalytic stage wherein the catalytic stage has a further catalyst and passing the contaminated gas stream serially through said photocatalytic stage by contacting the gas stream with the photocatalyst while irradiating the gas stream and the photocatalyst with UV radiation to convert a portion of the contaminants to oxidized species and thereafter passing the treated gas stream to a catalytic stage wherein the gas stream is passed over a catalyst so as to further convert the oxidized species and remaining contaminants to less harmful products. The gas

stream is irradiated in the photocatalytic stage with ultraviolet light having a wavelength of between 150 to about 400 nanometers and the contaminated gas stream has a residence time in the photocatalytic stage of between about .001 to about 5 seconds, where the residence time is defined as the ratio of the volume of the photocatalyst to the total volumetric flow rate of the contaminated gas stream. The process is carried out in the photocatalytic stage at a temperature of between about 20°F to 1200°F and a pressure of between about 0.2 atm to about 10 atm. The photocatalyst employed in the photocatalytic stage is a particular photocatalyst as described hereinbelow. The catalytic stage is operated at a temperature of between about 200°F and 1200°F and a pressure of between about .02 atm to 10 atm. The residence time of the gas stream in the catalytic stage is between .001 to about 5 seconds, where the residence time is defined as the ratio of the volume of the catalyst to the total volumetric flow rate of the gaseous stream. The details of the preferred catalyst employed in the catalytic stage is described hereinbelow.

The process of the present invention is both economic and efficient and superior to known processes.

Further objects and advantages of the present invention will appear from the detailed description.

DETAILED DESCRIPTION

The present invention provides a gaseous phase oxidation system, using only oxygen contained in the inlet to the process as the oxidant, which operates at a surprisingly lower contact time with higher selectivity than prior art photocatalytic systems. The absence of any added oxidant, such as ozone or hydrogen peroxide, provides a simpler, lower cost process. The contact time, defined as the ratio of the catalyst bulk volume to the volumetric flow rate of the entering fluid, is an important commercial parameter of the invention. A low contact time is equivalent to a low catalyst volume when processing a given flow rate of fluid. If the contact time is reduced by a factor of ten, not only is the required volume of catalyst reduced by a factor of ten, but also the number of UV lamps and ballasts are proportionately reduced and the size of the reactor is proportionately reduced. These latter considerations greatly reduce the cost of construction and operation of the photocatalytic fluid purification process of the present invention, compared to the prior art. As will be exemplified below, a photocatalytic contact time of less than 0.1 seconds can be utilized with the present invention, compared to contact times as high as 34 to 100 seconds with prior art titania photocatalysts. The

present invention thereby enables a surprisingly high 300 to 1000-fold size reduction and a proportionate cost reduction compared to that of the prior art. An improvement of this magnitude would not be expected by those skilled in the art.

It is believed that the exceptional results of the photocatalysts of the present invention are due to four characteristics of the invention:

(a) a high photocatalytic activity of the photocatalysts of the present invention, which oxidize at least a portion of the contaminant in the incoming air, thereby producing some oxygenated products along with a heat of reaction;

(b) the elevated temperature of the photocatalyst which results from this reaction heat release further increases the photocatalytic activity;

(c) the oxygenated products from the photocatalytic bed and remaining contaminants can be oxidized by the catalytic bed at lower temperatures than can the original parent contaminant; and

(d) the heat release to the following catalytic bed increases its operating temperature and thereby its activity for contaminant destruction. The overall result is the use of extremely short residence times, enabling the photocatalytic technology to emerge as a cost effective environmental control option for treating large volumes of contaminated air.

Further, the system can be operated to completely oxidize contaminants in an air stream thus avoiding byproducts, using inlet air at ambient temperatures instead of the requirement of preheating the air stream to, say, 600°F as required in conventional catalytic processing.

The process of the present invention comprises the steps of:

- (a) providing a photocatalytic stage having a photocatalyst and a source of UV radiation;
- (b) providing a catalytic stage downstream of the photocatalytic stage, the catalytic stage having a catalyst;
- (c) passing the contaminated gas stream through the photocatalytic stage by contacting the gas stream with the photocatalyst while irradiating the contaminated gas stream and the photocatalyst with UV radiation so as to oxidize at least a portion of said contaminants to an oxidized species;
- (d) removing the gas stream with the oxidized species of contaminants from the photocatalytic stage; and
- (e) passing the gas stream with oxidized species of contaminants through the catalytic stage by passing the stream over the catalyst at elevated temperature so as to further convert the oxidized species and remaining contaminants to less harmful biproducts.

In accordance with the process of the present invention, the process includes repeating steps (c) through (e) a plurality of times. Thus, the process provides a plurality of alternating photocatalytic and catalytic stages in series.

In accordance with a preferred embodiment of the present invention, the gas stream is irradiated with ultraviolet light in the photocatalytic stage wherein the ultraviolet light has a wavelength of between about 150 to about 400 nanometers, preferably between 250 to about 375 nanometers. The source of the ultraviolet light may be low pressure ultraviolet bulbs or medium pressure ultraviolet bulbs. Medium pressure ultraviolet bulbs are preferred when the photocatalytic stage is operated at a temperature of greater than about 200°F. In accordance with the process of the present invention, the photocatalytic stage is operated under the following conditions: a temperature of between about 20°F to about 1200°F, preferably 50°F to 1000°F and still more preferably between about 100°F to 800°F and a pressure of between about 0.2 atm to 10 atm, preferably between about 0.8 atm to about 1.5 atm. The residence time of the contaminated gas in the photocatalytic stage is preferably between about 0.001 to about 5 seconds and preferably between about 0.01 to 2 seconds, where the residence time is defined as the ratio of

the volume of photocatalyst to the total volumetric flow rate of the contaminated gas.

It has been found that the photocatalyst employed in the photocatalytic stage is critical for optimizing the process of the present invention. In accordance with the present invention the preferred photocatalyst is selected from the group consisting of:

(a) from about 0.01 to about 8.0 wt.% titania, from about 0.01 to about 8.0 wt.% zirconia, and balance essentially silica;

(b) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, balance essentially silica;

(c) from about 0.01 to about 8.0 wt.% titania, from about 0.01 to about 8.0 wt.% zirconia, and an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, balance essentially silica;

(d) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, and balance essentially titania;

(e) an element selected from the group consisting of gold, silver and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, and balance essentially titania; and

(f) from about 10.0 to about 50.0 wt.% tungsten oxide, from about 0.1 to about 70.0 wt.% silica, from about 30.0 to about 90.0 wt.% titania, and an element selected from the group consisting platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%.

A particularly preferred photocatalyst comprises titania, and an element selected from the group consisting of platinum, palladium and mixtures thereof. A particularly suitable photocatalyst is a photocatalyst which comprises from about 0.1 wt.% to about 70 wt.% silica, from about 30 wt.% to about 90 wt.% titania, from about 20 wt.% to about 30 wt.% tungsten oxide, and an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 wt.% to about 5.0 wt.%.

The second catalytic stage for the process of the present invention is operated under the following conditions: a temperature of between about 200°F to about 1200°F, preferably 300°F to 1000°F, and a pressure of between about 0.2 atm to about 10 atm, preferably, between about 0.8 atm to about 1.5 atm. The residence time of the gaseous stream with the

catalyst in the catalytic stage is between about .001 to about 5 seconds, preferably between about .01 to about 5 seconds, where the residence time is defined as the ratio of the volume of the catalyst to the total volumetric flow rate of the stream.

It has been found that the catalyst provided in the catalytic stage in accordance with the process of the present invention is critical in optimizing the efficiency of the process of the present invention. When the contaminated gas stream contains no halogens, preferred catalysts are selected from the group consisting of:

(a) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, and balance essentially a component selected from the group consisting of alumina, silica and mixtures thereof;

(b) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, and balance essentially titania;

(c) from about 10.0 to about 50.0 wt.% tungsten oxide, from about 0.1 to about 70.0 wt.% silica, from about 30.0 to about 90.0 wt.% titania, and an element selected from the

group consisting platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%; and

(d) from about 25 to about 90 wt.% manganese oxide, from about 0.5 to about 40 wt.% copper oxide and from about 0.5 to about 40 wt.% alumina.

When the catalyst defined in paragraph (d) above is employed, it is preferred that the manganese oxide, copper and alumina be coprecipitated. It has been found that the activity of catalyst (d) can be increased by coprecipitation rather than attempting to impregnate the alumina with the high wt.% of magnesium oxide.

When the contaminated gas contains halogen atoms, the preferred catalyst of the present invention is selected from the group consisting of:

(a) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, and balance essentially titania;

(b) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, balance essentially silica; and

(c) from about 10.0 to about 50.0 wt.% tungsten oxide, from about 0.1 to about 70.0 wt.% silica, from about 30.0 to

about 90.0 wt.% titania, and an element selected from the group consisting platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%.

When employing a catalyst containing silica, it has been found that silica gels are preferred. Preparation of silica gels are well known in the art as for example described in co-pending Application Serial Number 09/262,895 filed March 8, 1999 and assigned to the assignee of the instant invention.

The contaminated air may be contacted with the photocatalyst in the photocatalytic stage and the catalyst in the catalytic stage in any fashion known to those skilled in the art. Preferably, the fluid is passed over layered beds of the photocatalyst and/or catalyst with, in the photocatalytic stage, ultraviolet light sources being placed between the layered beds. An alternate configuration is to illuminate the photocatalyst by embedding the light bulbs in a packed bed of the photocatalyst, preferably when the light bulbs are enclosed in a quartz sleeve.

The catalyst of the present invention can be prepared by any method known in the prior art, such as impregnation, precipitation, or any other method known in the art.

Advantages of the present invention will be made clear from the following examples.

EXAMPLE 1

A stainless steel reactor with a cross section of about 6 inches by 10 inches was constructed, containing a top photocatalytic bed and a lower catalytic bed. Air flow containing the contaminant was introduced at the top of the reactor, flowing first through the photocatalytic bed and next through the catalyst bed. Five medium pressure UV bulbs were placed in a row above the photocatalyst bed, at a distance of about 0.5 inches above the photocatalyst. The wattage of the five bulbs placed along the 10 inch dimension of the reactor was 400, 340, 220, 340, and 400, for a total wattage of 1,700 watts. The photocatalyst bed was a depth of 1 inch, with a six inch by 10 inch cross section, or a total volume of 980 cc. The photocatalyst bed was titania pellets impregnated with platinum to a level of 1% by weight. After a five inch mixing zone below the photocatalyst bed, the contaminated air flowed through the catalyst bed, containing titania pellets impregnated with platinum to a level of 1% by weight. The depth of the catalyst bed was 5 inches, or a total volume of 4,900 cc.

Air at a temperature of 74°F was contaminated with pentane, to a concentration of 3,265 ppm by volume. The contaminated air was fed to the reactor at a rate of 22 cubic feet per minute, passing serially over the photocatalyst bed

and then the catalyst bed. With the UV lamps illuminated, 1,700 watts of electrical energy entered the reactor, which would be sufficient to heat the incoming contaminated air by about 200°F.

Measurements of the inlet and exit pentane concentration from the photocatalytic/catalytic reactor were made, showing an outlet pentane concentration of 1 ppm. Compared to the inlet concentration of 3,265 ppm, this represents a destruction efficiency of 99.97%. No byproducts were observed from the reactor exit gas analyses. The temperature profile in the system suggested that a substantial conversion was achieved in the photocatalytic bed, of over two-thirds of the total conversion, with the balance being achieved in the catalytic bed. The residence time in the photocatalytic bed is only 0.09 seconds, representing a space velocity of over 38,000 hr⁻¹.

The results are surprising and unexpected. The residence time of the photocatalytic bed is too small to expect substantial conversion, 0.09 seconds, because most photocatalysts require residence times of several seconds to be effective for even chlorinated hydrocarbons, which are easier to convert than is pentane. Further, the temperature of the air heated by the UV lamps is too low to expect substantial conversion in the catalyst bed. Yet, by combining

these two negative expectations, a highly positive result was achieved with 99.97% destruction efficiency without byproducts. It is believed that the photocatalyst is producing partially oxygenated byproducts, which are particularly easily converted in the catalytic section. In addition, the heat of reaction which is produced serves to elevate the temperature of both the photocatalyst and the catalyst sections to promote the rate of reaction, even though the overall energy input into the system was only 1,700 watts, or equal to a about 200°F temperature rise.

EXAMPLE 2

The reactor of Example 1 was employed to destroy methyl chloride in air, which is known to be a particularly difficult compound to oxidize by photocatalysis. An air stream of 7 SCFM was fed to the reactor of Example 1, containing 288 ppm (vol.) of methyl chloride. The reactor was operated under the conditions of Example 1. The observed destruction efficiency of methyl chloride was 99.5%, far higher than would be expected by the use of either photocatalysis or catalysis alone. Also, no byproducts were observed by analysis of the reactor effluent by gas chromatography.

EXAMPLE 3

The reactor of Example 1 was employed to destroy methylene chloride in air, which is known to be a particularly difficult compound to oxidize by photocatalysis. An air stream of 10 SCFM was fed to the reactor of Example 1, containing 369 ppm (vol.) of methylene chloride. The reactor was operated under the conditions of Example 1. The observed destruction efficiency of methylene chloride was 99.3%, far higher than would be expected by the use of either photocatalysis or catalysis alone. Also, no byproducts were observed by analysis of the reactor effluent by gas chromatography.

EXAMPLE 4

A stainless steel reactor with a cross section of 2 inches by 7.5 inches was constructed, containing a top photocatalytic bed and a lower catalytic bed. Air flow containing the contaminant was introduced at the top of the reactor, flowing first through the photocatalytic bed and next through the catalyst bed. One medium pressure, 400 watt UV bulb was placed above the photocatalyst bed, at a distance of about 0.5 inches above the photocatalyst. The photocatalyst bed was filled to a depth of about 1 inch, with a total weight of 131.2 grams. The photocatalyst bed composition was 0.012%

titania, 0.01% zirconia, 1% platinum, and the balance silica, all on a weight basis. After the photocatalyst bed, the contaminated air flowed through the catalyst bed, containing 632.1 grams of a catalyst of about 70% manganese dioxide, 12% copper oxide, and the balance alumina.

Air at a temperature of about 74°F was contaminated with hexane, to a concentration of 625 ppm by volume. The contaminated air was fed to the reactor at a rate of 1.9 cubic feet per minute, passing over the photocatalyst bed and then the catalyst bed.

Measurements of the inlet and exit hexane concentration from the photocatalytic/catalytic reactor were made, showing an outlet hexane concentration of 2.6 ppm. Compared to the inlet concentration of 625 ppm, this represents a destruction efficiency of 99.6%. No byproducts were observed from the reactor exit analyses.

EXAMPLE 5

The reactor of Example 4 was employed to destroy hexane in air, except the photocatalyst of Example 4 was replaced with the photocatalyst of Example 1. The catalyst of Example 4 was also used in this present Example 5. An air stream of 2.2 SCFM at about 70°F was fed to the reactor, containing 832 ppm (vol.) of mixed hexanes. The observed destruction

efficiency of hexanes was 99.9%. No byproducts were observed by analysis of the reactor effluent by gas chromatography.

The performance of this system is substantially superior to that expected by the use of either photocatalysis or catalysis alone under these experimental conditions. In particular, little destruction of hexanes to carbon dioxide is usually achieved by photocatalysis alone, and catalysis alone would require preheating the air to a temperature of over 600°F. The combination of the two steps with the claimed catalysts provides exceptional results.

This invention may be embodied in other forms or carried out in other ways without departing from the spirit or essential characteristics thereof. The present embodiment is therefore to be considered as in all respects illustrative and not restrictive, the scope of the invention being indicated by the appended claims, and all changes which come within the meaning and range of equivalency are intended to be embraced therein.

IN THE CLAIMS

1. A process for purifying a contaminated gas stream by conversion of the contaminants into less harmful products, comprising the steps of:

(a) providing a photocatalytic stage having a photocatalyst and a source of UV radiation;

(b) providing a catalytic stage downstream of said photocatalytic stage, said catalytic stage having a catalyst;

(c) passing said contaminated gas stream through said photocatalytic stage by contacting said gas stream with said photocatalyst while irradiating said contaminated gas stream and photocatalyst with UV radiation so as to oxidize at least a portion of said contaminants to an oxidized species;

(d) removing said gas stream with said oxidized species of contaminants from said photocatalytic stage; and

(e) passing said gas stream with oxidized species of contaminants through said catalytic stage by passing said stream over said catalyst at elevated temperatures so as to further convert said oxidized species and remaining contaminants to less harmful products.

2. A process according to claim 1, further including the steps of repeating steps (c) through (e) a plurality of times.

3. A process according to claim 1, further including providing a plurality of alternating photocatalytic and catalytic stages in series.

4. A process according to claim 1, wherein said gas stream in said photocatalytic stage is irradiated with ultraviolet light having a wave length of about 150 to about 400 nanometers.

5. A process according to claim 4, wherein said wavelength is between about 250 to about 375 nanometers.

6. A process according to claim 4, wherein said contaminated gas stream has a residence time in said photocatalytic stage of between about .001 to about 5 seconds, where the residence time is defined as the ratio of the volume of the photocatalyst to the total volumetric flow rate of said contaminated gas stream.

7. A process according to claim 4, wherein said contaminated gas stream has a residence time in said photocatalytic stage of between about 0.01 to about 2 seconds, where the residence time is defined as the ratio of the volume of the photocatalyst to the total volumetric flow rate of said contaminated gas stream.

8. A process according to claim 6, wherein the process is carried out in the photocatalytic stage under the following conditions: a temperature of between about 20°F to about 1200°F; a pressure of between about 0.2 atm to about 10 atm.

9. A process according to claim 6, wherein the process is carried out in the photocatalytic stage under the following conditions: a temperature of between about 50°F to about 1000°F; a pressure of between about 0.8 atm to about 1.5 atm.

10. A process according to claim 6, wherein the process is carried out in the photocatalytic stage under the following conditions: a temperature of between about 100°F to about 800°F; a pressure of between about 0.8 atm to about 1.5 atm.

11. A process according to claim 1, wherein said photocatalyst is selected from the group consisting of:

(a) from about 0.01 to about 8.0 wt.% titania, from about 0.01 to about 8.0 wt.% zirconia, and balance essentially silica;

(b) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, balance essentially silica;

(c) from about 0.01 to about 8.0 wt.% titania, from about 0.01 to about 8.0 wt.% zirconia, and an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, balance essentially silica;

(d) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, and balance essentially titania;

(e) an element selected from the group consisting of gold, silver and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, and balance essentially titania; and

(f) from about 10.0 to about 50.0 wt.% tungsten oxide, from about 0.1 to about 70.0 wt.% silica, from about 30.0 to about 90.0 wt.% titania, and an element selected from the

group consisting platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%.

12. A process according to claim 1, wherein said photocatalyst comprises titania and an element selected from the group consisting of platinum, palladium and mixtures thereof.

13. A process according to claim 1, wherein said photocatalyst comprises from about 0.1 wt.% to about 70 wt.% silica, from about 30 wt.% to about 90 wt.% titania, and from about 10 wt.% to about 50 wt.% tungsten oxide.

14. A process according to claim 13, wherein said tungsten oxide is present in an amount of between about 20 wt.% to about 30 wt.%.

15. A process according to claim 13, wherein said photocatalyst further includes an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 wt.% to about 50 wt.%.

16. A process according to claim 6, wherein said gas stream with said partially oxidized species of contaminants

has a residence time in said catalytic stage of between about .001 to about 5 seconds, where the residence time is defined as the ratio of the volume of the catalyst to the total volumetric flow rate of said stream.

17. A process according to claim 7, wherein said gas stream with said partially oxidized species of contaminants has a residence time in said catalytic stage of between about .01 to about 5 seconds, where the residence time is defined as the ratio of the volume of the catalyst to the total volumetric flow rate of said stream.

18. A process according to claim 16, wherein the process is carried out in the catalytic stage under the following conditions: a temperature of between about 200°F to about 1200°F; a pressure of between about 0.2 atm to about 10 atm.

19. A process according to claim 17, wherein the process is carried out in the catalytic stage under the following conditions: a temperature of between about 300°F to about 1000°F; a pressure of between about 0.8 atm to about 1.5 atm.

20. A process according to claim 1 wherein said catalyst is selected from the group consisting of:

(a) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, and balance essentially a component selected from the group consisting of alumina, silica and mixtures thereof

(b) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, and balance essentially titania;

(c) from about 10.0 to about 50.0 wt.% tungsten oxide, from about 0.1 to about 70.0 wt.% silica, from about 30.0 to about 90.0 wt.% titania, and an element selected from the group consisting platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%; and

(d) from about 25 to about 90 wt.% manganese oxide, from about 0.5 to about 40 wt.% copper oxide and from about 0.5 to about 40 wt.% alumina.

21. A process according to claim 1, wherein said catalyst comprises from about 0.1 wt.% to about 70 wt.% silica, from about 30 wt.% to about 90 wt.% titania, and from about 10 wt.% to about 50 wt.% tungsten oxide.

22. A process according to claim 21, wherein said tungsten oxide is present in an amount of between about 20 wt.% to about 30 wt.%.

23. A process according to claim 22, wherein said catalyst further includes an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 wt.% to about 50 wt.%.

24. A process according to claim 1, wherein said contaminated gas stream contains halogen atoms and said catalyst is selected from the group consisting of:

(a) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, and balance essentially titania;

(b) an element selected from the group consisting of platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%, balance essentially silica;

(c) from about 10.0 to about 50.0 wt.% tungsten oxide, from about 0.1 to about 70.0 wt.% silica, from about 30.0 to about 90.0 wt.% titania, and an element selected from the

group consisting platinum, palladium and mixtures thereof in an amount of between about 0.01 to about 5.0 wt.%.

25. An apparatus for purifying a contaminated gas stream comprising:

(a) a first stage photocatalytic reaction zone having a source of ultraviolet light and a photocatalyst;

(b) a second stage catalytic reaction zone downstream of said first stage, said second stage having a catalyst; and

(c) means for feeding the gas stream serially through said first stage and said second stage.

26. An apparatus according to claim 25, including a plurality of alternating photocatalytic and catalyst stages in series.

ABSTRACT

A process comprises passing a contaminated gaseous stream through a photocatalytic stage and, thereafter, through a catalytic stage.

(Rev. 5-8-11/93 Pub. 605)

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PATENT

Attorney's Docket No. 99-323

COMBINED DECLARATION AND POWER OF ATTORNEY

(ORIGINAL, DESIGN, NATIONAL STAGE OF PCT, SUPPLEMENTAL, DIVISIONAL,
CONTINUATION OR CIP)

As a below named inventor, I hereby declare that:

TYPE OF DECLARATION

This declaration is of the following type: (check one applicable item below)

- ☒ original
☐ design
☐ supplemental

NOTE: If the declaration is for an International Application being filed as a divisional, continuation or continuation-in-part application, do not check next item; check appropriate one of last three items.

- ☐ national stage of PCT

NOTE: If one of the following 3 items apply, then complete and also attach **ADDED PAGES FOR DIVISIONAL, CONTINUATION OR CIP.**

- ☐ divisional
☐ continuation
☐ continuation-in-part (CIP)

INVENTORSHIP IDENTIFICATION

WARNING: If the inventors are each not the inventors of all the claims, an explanation of the facts, including the ownership of all the claims at the time the last claimed invention was made, should be submitted.

My residence, post office address and citizenship are as stated below next to my name. I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled:

TITLE OF INVENTION

TWO STAGE PROCESS AND APPARATUS FOR PHOTOCATALYTIC AND CATALYTIC
CONVERSION OF CONTAMINANTS

SPECIFICATION IDENTIFICATION

the specification of which: (complete (a), (b) or (c))

- (a) ☒ is attached hereto.
(b) ☐ was filed on _____ as ☐ Serial No. 0 / _____
or ☐ Express Mail No., as Serial No. not yet known _____
and was amended on _____ (if applicable).

NOTE: Amendments filed after the original papers are deposited with the PTO which contain new matter are not accorded a filing date by being referred to in the declaration. Accordingly, the amendments involved are those filed with the application papers or, in the case of a supplemental declaration, are those amendments claiming matter not encompassed in the original statement of invention or claims. See 37 CFR 1.67.

- (c) ☐ was described and claimed in PCT International Application No. _____
filed on _____ and as
amended under PCT Article 19 on _____ (if any).

(Declaration and Power of Attorney [1-1]—page 1 of 5)

ACKNOWLEDGEMENT OF REVIEW OF PAPERS AND DUTY OF CANDOR

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose information

- ☒ which is material to patentability as defined in 37, Code of Federal Regulations, § 1.56

(also check the following items, if desired)

- ☒ and which is material to the examination of this application, namely, information where there is a substantial likelihood that a reasonable examiner would consider it important in deciding whether to allow the application to issue as a patent, and
- ☐ in compliance with this duty there is attached an information disclosure statement in accordance with 37 CFR 1.98.

PRIORITY CLAIM (35 U.S.C. § 119)

I hereby claim foreign priority benefits under Title 35, United States Code, § 119 of any foreign application(s) for patent or inventor's certificate or of any PCT International application(s) designating at least one country other than the United States of America listed below and have also identified below any foreign application(s) for patent or inventor's certificate or any PCT International application(s) designating at least one country other than the United States of America filed by me on the same subject matter having a filing date before that of the application(s) of which priority is claimed.

(complete (d) or (e))

- (d) ☒ no such applications have been filed.
- (e) ☐ such applications have been filed as follows.

NOTE: Where item (e) is entered above and the International Application which designated the U.S. itself claimed priority check item (e), enter the details below and make the priority claim.

A. PRIOR FOREIGN/PCT APPLICATION(S) FILED WITHIN 12 MONTHS (6 MONTHS FOR DESIGN) PRIOR TO THIS APPLICATION AND ANY PRIORITY CLAIMS UNDER 35 U.S.C. § 119

COUNTRY (OR INDICATE IF PCT)	APPLICATION NUMBER	DATE OF FILING (day, month, year)	PRIORITY CLAIMED UNDER 37 USC 119
			<input type="checkbox"/> YES <input type="checkbox"/> NO
			<input type="checkbox"/> YES <input type="checkbox"/> NO
			<input type="checkbox"/> YES <input type="checkbox"/> NO
			<input type="checkbox"/> YES <input type="checkbox"/> NO
			<input type="checkbox"/> YES <input type="checkbox"/> NO

(Declaration and Power of Attorney [1-1]—page 2 of 5)

(24-11/93 Pub.605)

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**ALL FOREIGN APPLICATION(S), IF ANY FILED MORE THAN 12 MONTHS
(6 MONTHS FOR DESIGN) PRIOR TO THIS U.S. APPLICATION**

NOTE: If the application filed more than 12 months from the filing date of this application is a PCT filing forming the basis for this application entering the United States as (1) the national stage, or (2) a continuation, divisional, or continuation-in-part, then also complete ADDED PAGES TO COMBINED DECLARATION AND POWER OF ATTORNEY FOR DIVISIONAL, CONTINUATION OR CIP APPLICATION for benefit of the prior U.S. or PCT application(s) under 35 U.S.C. § 120.

POWER OF ATTORNEY

I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application and transact all business in the Patent and Trademark Office connected therewith. (List name and registration number)

Robert H. Bachman (19,374)	all members of the firm
Gregory P. LaPointe (28,395)	Bachman & LaPointe, P.C.
Barry L. Kelmachter (29,999)	
George A. Coury (34,309)	

(check the following item, if applicable)

- ☐ Attached as part of this declaration and power of attorney is the authorization of the above-named attorney(s) to accept and follow instructions from my representative(s).

SEND CORRESPONDENCE TO

Gregory P. LaPointe
Bachman & LaPointe, P.C.
900 Chapel Street, Suite 1201
New Haven, CT 06510-2802

DIRECT TELEPHONE CALLS TO:
(Name and telephone number)

Gregory P. LaPointe
(203) 777-6628

DECLARATION

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code, and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

SIGNATURE(S)

NOTE: Carefully indicate the family (or last) name as it should appear on the filing receipt and all other documents.

Full name of sole or first inventor

James R. Kittrell
(GIVEN NAME) (MIDDLE INITIAL OR NAME) FAMILY (OR LAST NAME)
Inventor's signature James R. Kittrell
Date June 3, 1999 Country of Citizenship U.S.A.
Residence U.S.A.
Post Office Address 218 Heatherstone Road
Amherst, Massachusetts 01002

Full name of second joint inventor, if any

(GIVEN NAME) (MIDDLE INITIAL OR NAME) FAMILY (OR LAST NAME)
Inventor's signature _____
Date _____ Country of Citizenship _____
Residence _____
Post Office Address _____

Full name of third joint inventor, if any

(GIVEN NAME) (MIDDLE INITIAL OR NAME) FAMILY (OR LAST NAME)
Inventor's signature _____
Date _____ Country of Citizenship _____
Residence _____
Post Office Address _____

(Declaration and Power of Attorney [1-1]—page 4 of 5)

(Oct 58-11/93 Pub 605)

FORM 1-1

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CHECK PROPER BOX(ES) FOR ANY OF THE FOLLOWING ADDED PAGE(S) WHICH FORM A PART OF THIS DECLARATION

☐ Signature for third and subsequent joint inventors. Number of pages added _____

☐ Signature by administrator(trix), executor(trix) or legal representative for deceased or incapacitated inventor. Number of pages added _____

☐ Signature for inventor who refuses to sign or cannot be reached by person authorized under 37 CFR 1.47. Number of pages added _____

☐ Added page for signature by one joint inventor on behalf of deceased inventor(s) where legal representative cannot be appointed in time (37 CFR 1.47).

☐ Added pages to combined declaration and power of attorney for divisional, continuation, or continuation-in-part (C-I-P) application.

☐ Number of pages added _____

☐ Authorization of attorney(s) to accept and follow instructions from representative.

(If no further pages form a part of this Declaration, then end this Declaration with this page and check the following item:)

☒ This declaration ends with this page.